

ECE 488 – Automatic Control

PID Control

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Compulsory Course in Electronic and Communication
Engineering
Credits (3/0/3)

Course Webpage: <http://ECE488.cankaya.edu.tr>

Reminder

Reminder

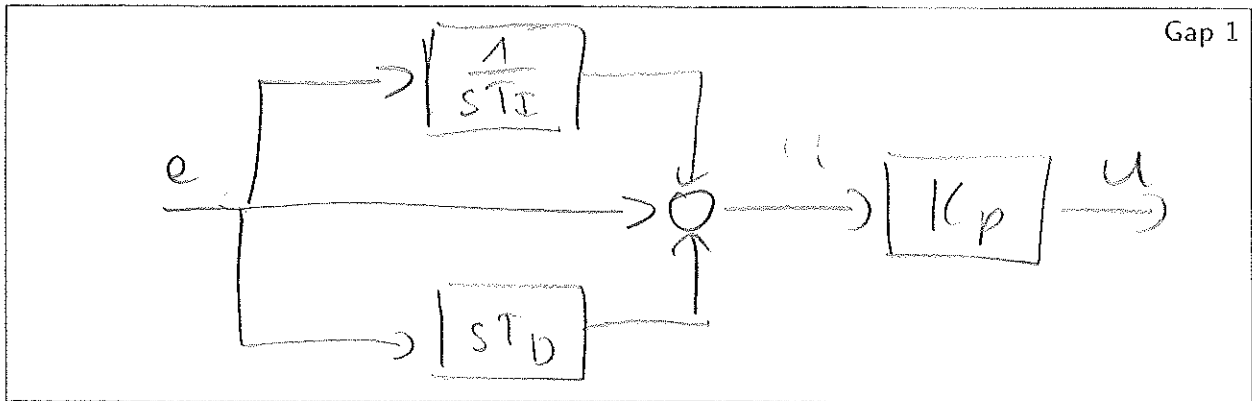
Previous Weeks

- LTI system modeling
- Nonlinear modeling and linearization
- Stability
- Steady-state and transient response
- Feedback Control
 - Root locus
 - Nyquist plot
- Bode plot and Lead/lag compensation

This week

- PID controller
- PID design

PID Controller: Characteristics



Gap 1

Ordinary Differential Equation (ODE)

$$u = K_p \cdot \left(e + \frac{1}{T_I} \int e + T_D \dot{e} \right)$$

Transfer Function (TF)

$$U(s) = K_p \cdot \left(E(s) + \frac{1}{T_I s} E(s) + T_D s E(s) \right) = K_p \left(1 + \frac{1}{T_I s} + T_D s \right) E(s)$$

PID Controller: Parameters

Proportional Action: $K_p \cdot e$

- Depends on instantaneous value of error
- Can control any stable plant but usually with low performance

Integral Action: $\frac{K_p}{T_I} \cdot \int e$

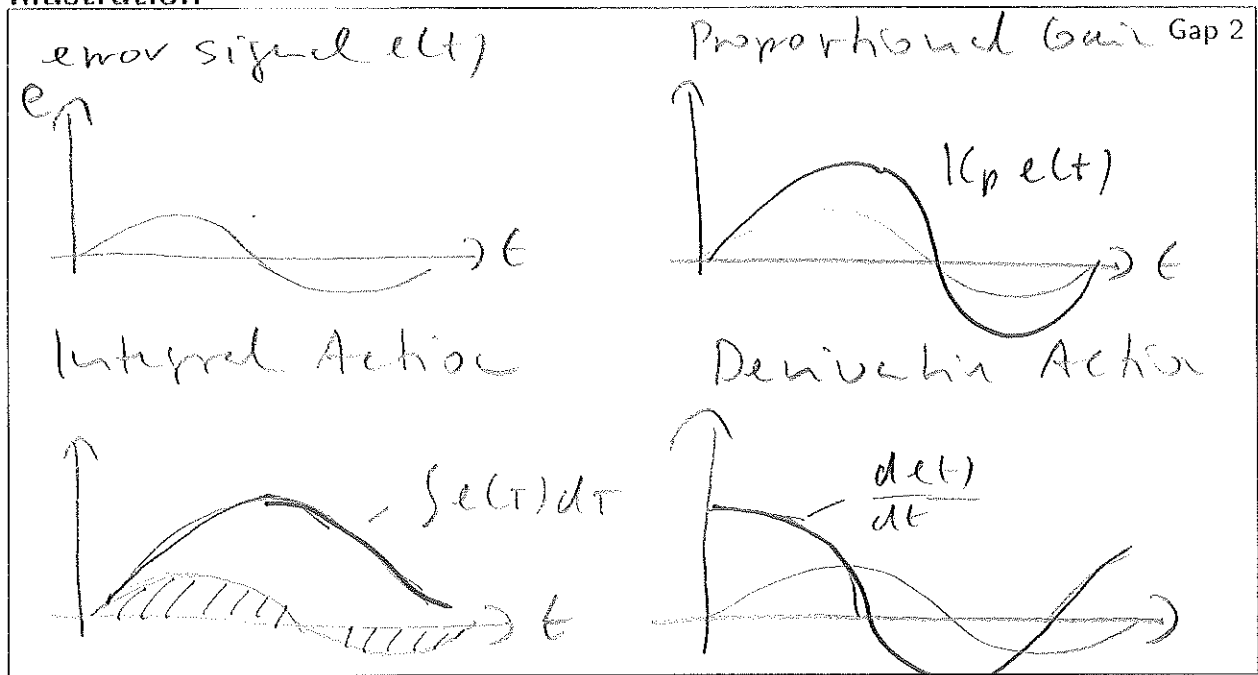
- Realizes memory due to dependency on accumulated error
- Enforces steady state error of $\lim_{t \rightarrow \infty} e(t) = 0$

Derivative Action: $K_p T_D \cdot \dot{e}$

- Captures trend of the error due to dependency on rate of change of e
- Susceptible to amplification of high-frequency disturbances/noise

PID Controller: Parameters

Illustration



PID Controller: Special Cases

PI-Controller

$$C(s) = K_p \left(1 + \frac{1}{T_I s} \right)$$

PD-Controller

$$C(s) = K_p (1 + T_D s)$$

Design Task

- Determine the most suitable controller type and the controller parameters K_p , T_I and T_D in order to fulfill given performance specifications

Ziegler-Nichols: Oscillation Method

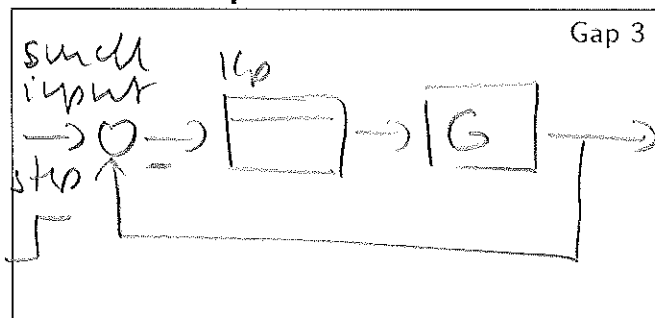
Assumption

- Stable, non-oscillatory plant: $G(s) = K \frac{e^{-s\tau}}{(1 + sT_1) \cdots (1 + sT_n)}$
excluding first-order/second-order lag
- Note: plant is not modeled!

Practical Experiment

- Start with $K_p = 0$ and increase K_p gradually until y oscillates
- Note critical gain $K_{crit} = K_p$
- Note oscillation period T_{crit}

Control Loop with P-control



Ziegler-Nichols: Oscillation Method

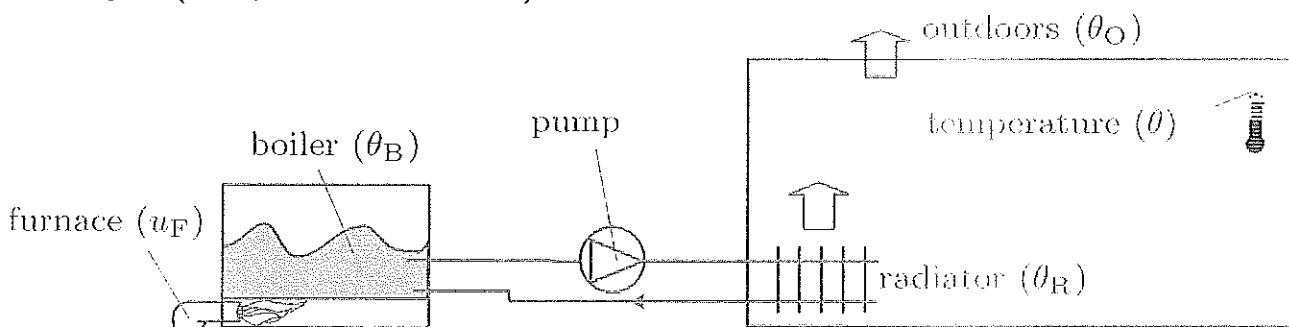
PID-controller Parameters

Controller	K_p	T_I	T_D
P-	$0.5K_{crit}$	∞	0
PI-	$0.45K_{crit}$	$0.85T_{crit}$	0
PID-	$0.6K_{crit}$	$0.5T_{crit}$	$0.12T_{crit}$

Results

- Stable closed loop
- Addresses both reference tracking and disturbance rejection

Example (temperature control)



Ziegler-Nichols: Example

Room temperature example

Read $K_{crit} = 4.8$ | $T_{crit} = 3.8$

Gap 4

P-control

$$K_p = 2.4$$

$$T_D = \infty$$

$$T_I = 0$$

PI-control

$$K_p = 2.2$$

$$T_I = 6.6$$

$$T_D = 0$$

PID-control

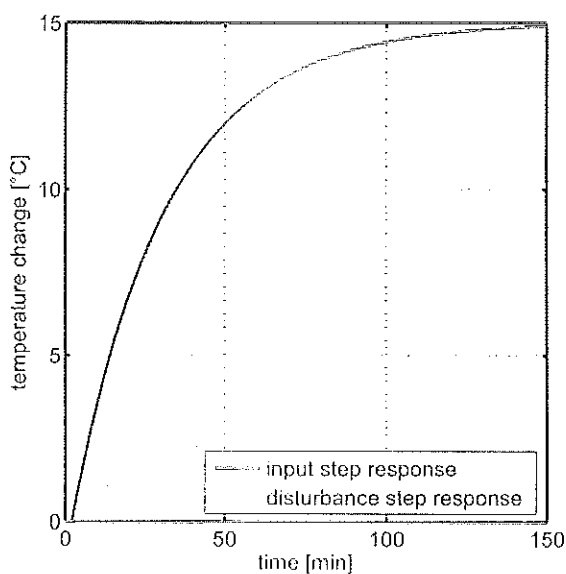
$$K_p = 2.5$$

$$T_I = 3.2$$

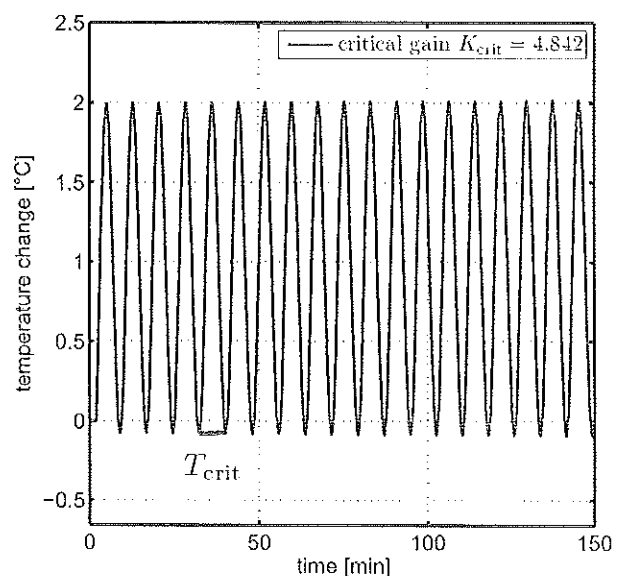
$$T_D = 0.5$$

Ziegler-Nichols: Oscillation Method

Uncontrolled Plant Step Response

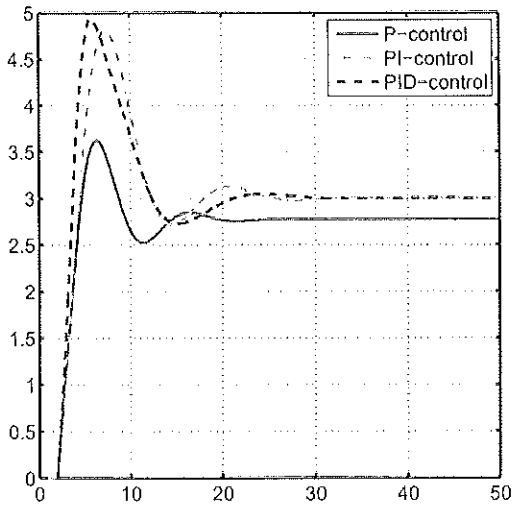


Oscillation Experiment

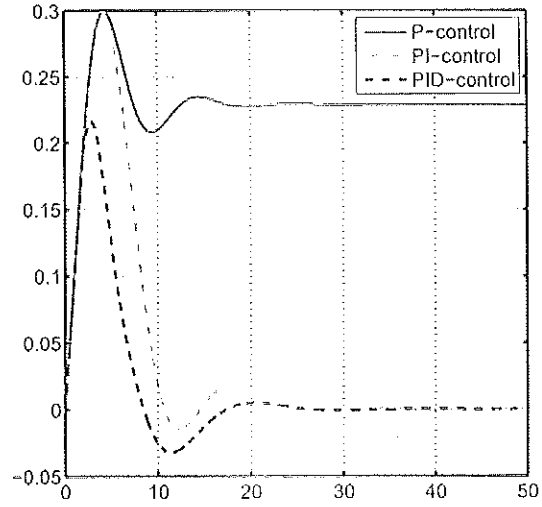


Ziegler-Nichols: Oscillation Method

Reference Step Response



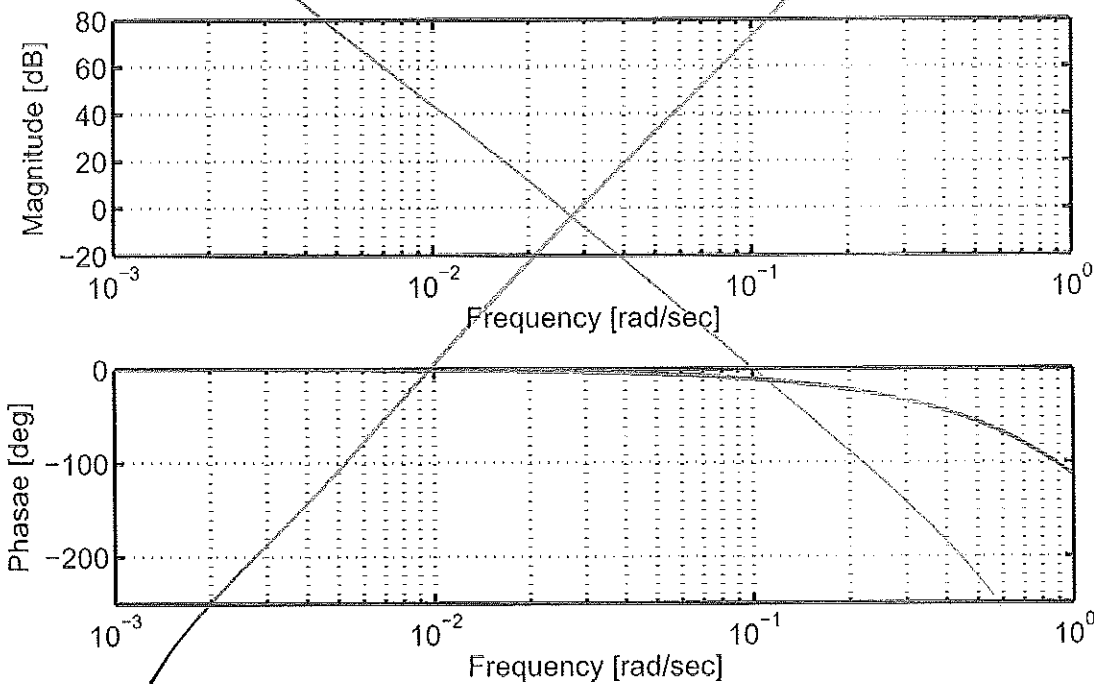
Disturbance Step Response



- ⇒ No exact following with P-control
- ⇒ Larger overshoot for PI and PID control due to plant delay
- ⇒ Similar dynamics for reference tracking and disturbance rejection

Ziegler-Nichols: Bode Plot

PI, show plot



Ziegler-Nichols: Example

Computation

$$\Phi_m = 35^\circ$$

Gap 5

$$\omega_g = -0.45 \text{ rad/sec}$$

\Rightarrow stable but oscillatory, lightly damped

Remarks

- Parameter computation for stability and sufficient phase margin
- Bandwidth of the closed loop according to gain crossover frequency
- Slope around the gain crossover frequency is -20 dB
- Further tuning of parameters is possible for example with Bode plot

Ziegler-Nichols: Example

Computation

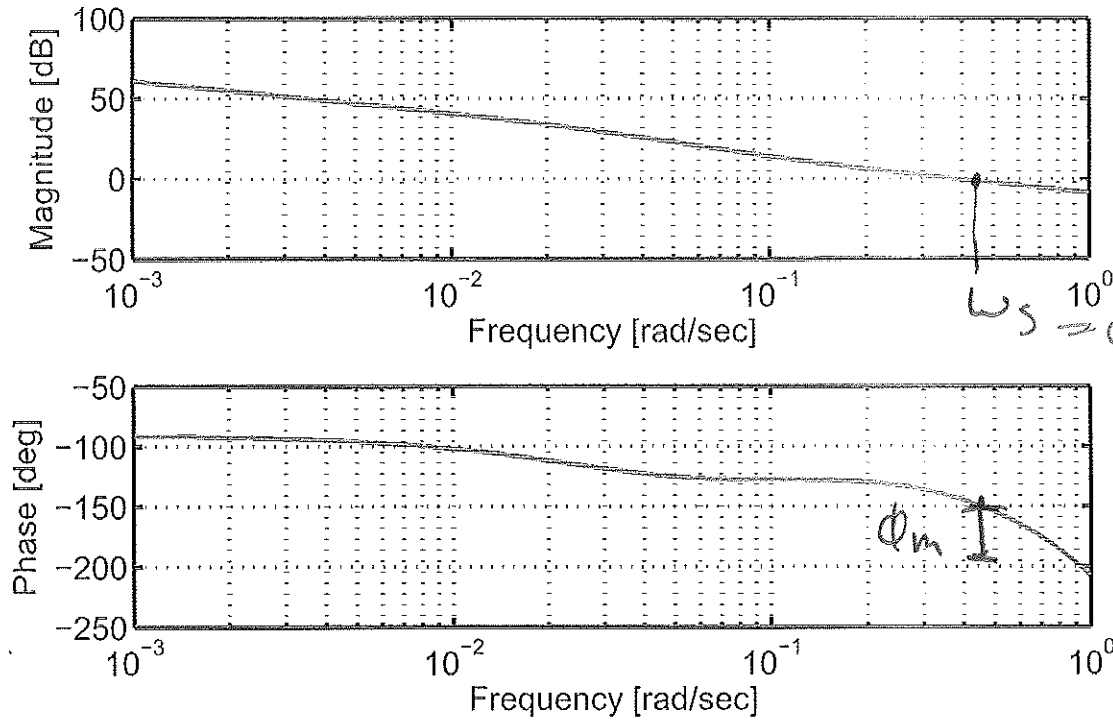
Gap 6

idea: decrease ω_g to increase Φ_m

\Rightarrow for example decrease gain and increase T_I

$$C(s) = \frac{1+10s}{10s}$$

Ziegler-Nichols: Bode Plot



Ziegler-Nichols: Reaction Curve Method

Assumption

- Stable, non-oscillatory plant: $G(s) = K \frac{e^{-sT}}{(1 + sT_1) \cdots (1 + sT_n)}$

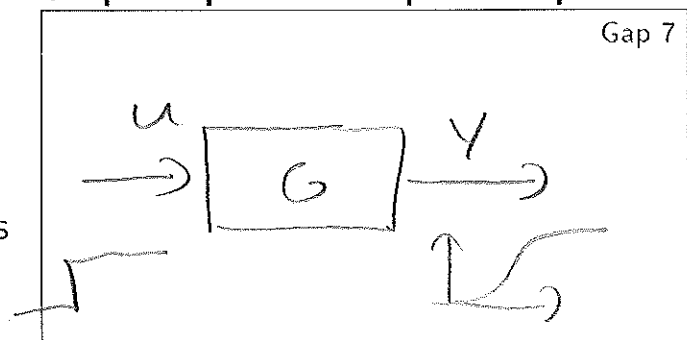
excluding $G(s) = \frac{K}{1 + sT_1}$

- Note: plant is not modeled!

Practical Experiment

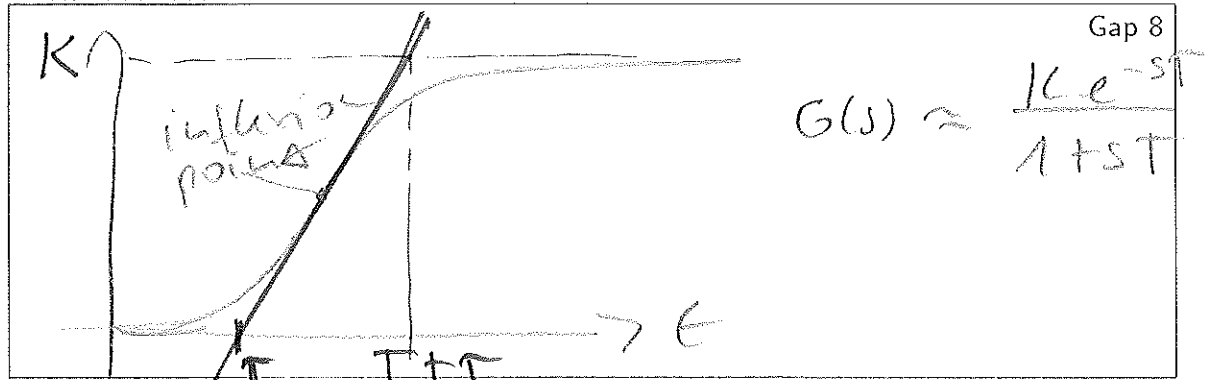
- Approach desired operating point
- Apply "small" step input
- Record plant output: process reaction curve

Step Response in Open Loop



Ziegler-Nichols: Reaction Curve Method

Characteristic Plant Parameters

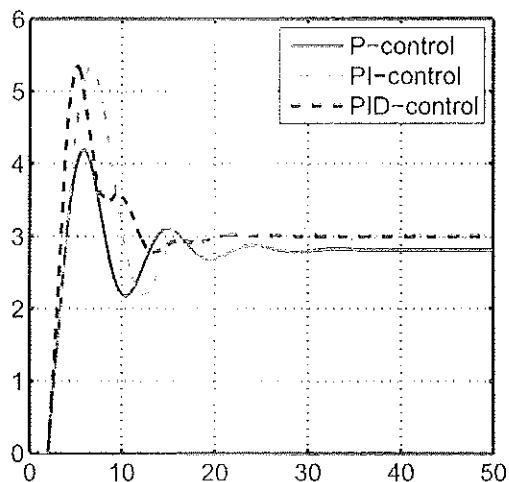


PID-controller Parameters

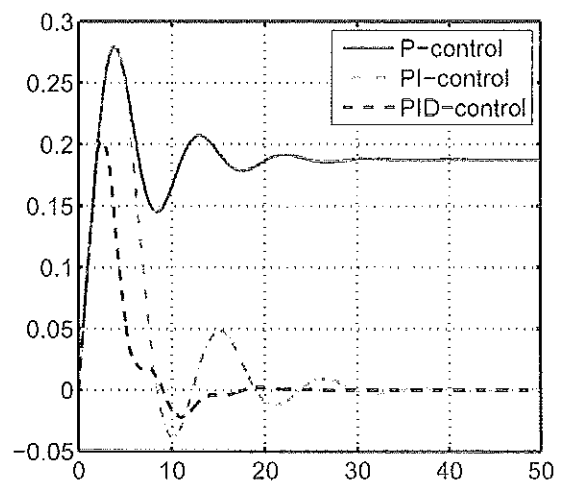
Controller	K_p	T_I	T_D
P-	$1/K \cdot T/\tau$	∞	0
PI-	$0.9/K \cdot T/\tau$	$3.33T$	0
PID-	$1.2/K \cdot T/\tau$	$2T$	$0.5T$

Ziegler-Nichols: Oscillation Method

Reference Step Response



Disturbance Step Response



⇒ Similar behavior to Ziegler-Nichols Oscillation Method

Ziegler-Nichols: Concluding Remarks

Usage

- Stable non-oscillatory plants
- No mathematical model required
- Oscillation or step response experiments
- Design of P, PI and PID-controllers
- Stable closed loop

Limitations

- Requires certain plant characteristics
- Empirical design should be followed by fine tuning on physical system
- Usage of integral control can lead to large overshoot for delay plants

More PID Design Methods

- For example, ECE 441, ECE 438